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**UNITED STATES PATENT APPLICATION**

of

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for

**METHOD AND APPARATUS  
FOR INTRODUCING SULPHUR DIOXIDE  
INTO AQUEOUS SOLUTIONS**

## BACKGROUND OF THE INVENTION

### 1. Related Application

Filed Aug. 21, 2000  
now U.S. Patent No. 6,506,347

This application is a continuation-in-part of Patent Application Serial No. 09/643,097  
which is a continuation-in-part of Patent Application Serial No. 08/888,376 filed on Jul. 7, 1997

### 2. The Field of the Invention

now U.S. Patent No. 6,248,299

Only a fraction of the earth's total water supply is available and suitable for agriculture, industry and domestic needs. The demand for water is great and new technologies together with growing populations increase the demand for water while pollution diminishes the limited supply of usable water. The growing demand for water requires efficient use of available water resources.

Agricultural use of water places a large demand on the world's water supply. In some communities, the water supply may be adequate for farming but the quality of the water is unsuitable for agriculture because the water is alkaline. Alkalinity is an important factor affecting the quality, efficiency and performance of soil and irrigation water. A relative increase in irrigation alkalinity due to the water's sodium to calcium ratio or a high pH renders irrigation water detrimental to soil, crop growth and irrigation water efficiency. Such water can be reclaimed for soil rehabilitation and irrigation by adding lower pH sulphur acid or sulphurous acid to the alkaline water to reduce its alkalinity or pH.

Use and quality of culinary water is also rising. In most populated areas, treatment of water for culinary and household use is necessary. Many water treatment facilities use various forms of chlorine to kill bacteria in the water. A necessary step in such processes include subsequently removing residual chlorine before introducing the treated water back into streams or rivers or into public culinary water systems.

The invention of this application is directed toward a device which generates quantities of sulphur dioxide gas or sulphur acid in a simplified, controllable, safe and efficient way. In

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particular, it is directed toward a sulphur dioxide or sulphurous acid generator which produces sulphurous compounds by burning elemental sulphur to produce sulphur gases. The sulphur gases are then drawn toward and held in contact with water eventually reacting with the water and producing sulphur acids, while substantially reducing dangerous emissions of sulphur gases to the air.

### 3. The Relevant Technology

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There are several sulphurous acid generators in the art. The prior art devices utilize sulphur burn chambers and absorption towers. However, known systems utilize countercurrent current flow or pressurized systems as the principle means to accomplish the generation of sulphurous acid. For example, many devices employ the absorption tower to introduce the majority of the water to the system in countercurrent flow to the flow of sulphur dioxide gas. United States Patent No. 4,526,771 teaches introducing 90% of the system water for the first time in countercurrent flow at the top of the absorption tower. In such devices, the integrity of the absorption towers is vital, and any deficiencies or inefficiencies of the absorption tower lead to diminished reaction and results. Other devices utilize pressurized gas to facilitate flow of gas through the system, see United States Patent No. 3,226,201. Pressurized devices, however, require expensive manufacture to ensure the containment of dangerous sulphur dioxide gas to avoid leakage. Even negative pressure machines have the drawback of requiring a source of energy to power the negative pressure generator such as an exhaust fan. Still other devices rely upon secondary combustion chambers to further oxidize the sulphur, see United States Patent No. 4,526,771. Many sulphurous acid generators emit significant or dangerous levels of unreacted sulphur dioxide gas, a harmful and noxious pollutant, into the surrounding environment.

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Known processes exist for dechlorinating water. These processes typically employ storage, containment and use of liquid or pressurized sulphur gases to remove harmful chlorine compounds from the water. Many of the known systems require expenses and large

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transportation and storage needs such as trains, train tracks, tankers, tanks, semitrucks and other equipment. Liquid and pressurized sulphur gases are hazardous and require elaborate and regulated usage and handling as well as hazardous release evacuation plans and specialized training of personnel and coordination with public health and safety officials, officers and servants.

What is needed is a method and apparatus for on-site, safe and controllable generation of needed sulphur gases. What is needed are methods and apparatuses which alleviate the need for expensive equipment or machinery for the transportation, storage and use of sulphur gases. What is needed is an onsite sulphur gas generator which can supply needed sulphur gases on demand without the need for expensive and elaborate hazardous material management and emergency contingencies.

#### **SUMMARY AND OBJECTS OF THE INVENTION**

The present invention is directed to a sulphur gas generator which can be used to improve alkaline irrigation water, dechlorinate water or treat landfill deposits. By adding sulphur gases or sulphur acids to alkaline water, the alkalinity and/or pH of the water is reduced. In addition to making the water less alkaline, adding sulphur acids to alkaline water increases the availability of sulphur in the water to act as a nutrient, improves capillary action of the soil, increases cation exchange capacity, and decreases tail water run-off and tillage and fertilizer costs. For purposes of this patent the term “sulphurous acid” shall mean ultimate and intermediate acids of sulphur created when sulphur gases created by combustion of sulphur react or mix with aqueous solution.

In many agricultural settings, complicated farm machinery is not practical because it requires technical training to operate and special skills to service and maintain. For sulphur gas generators, improved design can reduce costs, simplify operation, service and maintenance and increase efficiency and safety thereby making the machine more practical for agricultural use.

The present invention is directed toward a sulphur gas generator that is simple to produce, operate, service and maintain, and which efficiently produces, contains and reacts sulphur dioxide gas, and sulphurous acid if desired, without exposing the user or other living things in proximity to the machine to dangerous sulphur dioxide emissions.

5 It will be appreciated that a specific energy source is not necessarily required by the present invention, and therefore its use is not necessarily restricted to locations where a particular power source, like electricity, is available or can be generated for use. All of the above objectives are met by the present invention.

10 Unlike the prior art, the present invention is designed to generate, regulate and control the amount of sulphur dioxide gas generated on-site and on-demand for the combustion of elemental sulphur or sulfur and the duration of the contact of water with sulphur gases without creating or by minimizing back pressure in the system or without relying upon pressurization of the gas to cause the sulphur dioxide gas to flow through the generator or for introduction of the gas into aqueous solution. This reduces the complexity of the sulphur gas generator and the need for additional equipment such as air compressors used by prior art devices, or transportation, storage and other equipment typically associated with the use of liquid or pressurized sulphur gases.

15 The invention primarily relates to a sulphur hopper, a burn chamber and a gas pipeline. Additionally, an injector, a mixing tank, an exhaust pipeline, and an exhaust scrubbing tower may be employed.

20 The sulphur hopper preferably has a capacity of several hundred pounds of sulphur in powder, flake, split-pea or pastile form. The sulphur hopper can be constructed of various materials or combinations thereof. In one embodiment, the sulphur hopper is constructed of stainless steel and plastic. In the preferred embodiment the hopper is constructed of Sagggregate™ concrete. The sulphur hopper is connected to the burn chamber by a passageway positioned at the base of the sulphur hopper. The conduit joins the burn chamber at its base.

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The weight of the sulphur in the sulphur hopper forces sulphur through the passageway at the base and into the burn chamber, providing a continual supply of sulphur for burning.

A cooling ring is disposed at the base of the hopper. The cooling ring enters the base of the hopper, traverses a u-shaped pattern near the passageway into the burn chamber protruding above the base of the hopper. The cooling ring creates a physical and temperature barrier preventing molten sulphur from flowing across the entire base of the hopper.

The burn chamber has an ignition inlet on the top of the burn chamber through which the sulphur is ignited and an air inlet on the side of the chamber through which oxygen enters to fuel the burning sulphur. The burning sulphur generates sulphur dioxide gas. In the preferred embodiment, the top of the chamber is removable, facilitating access to the chamber for maintenance and service. The burn chamber is constructed of material capable of withstanding the corrosiveness of the sulphur and the heat of combustion, namely stainless steel but preferably Sagggregate™ concrete. Sagggregate™ concrete is preferred because it significantly decreases the cost of the hopper and burning chamber. Sagggregate™ concrete is a unique blend of cement and aggregates.

Sulphur dioxide gas exits the burn chamber through an exhaust outlet on the top of the burn chamber and is drawn into a first conduit. The first conduit may be manufactured from stainless steel. The sulphur dioxide gas may be directly injected or released into aqueous solution.

#### Optional Features

If the sulphur dioxide is not directly injected or released into aqueous solution, a supply of water is conducted by a second conduit and may be brought from a water source through the second conduit by any means capable of delivering sufficient water and pressure, such as an elevated water tank or a mechanical or electric pump.

The first conduit and second conduit meet and couple with a third conduit. The third conduit may comprise a blending portion, a contact containment portion, an agitation portion

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and a means for discharging the sulphurous acid and unreacted sulphur dioxide gas. In the third conduit, the sulphur dioxide gas and water are brought in contact with each other to form sulphurous acid. The third conduit may be constructed of polyethylene plastic, pvc or any durable plastic.

5       The blending portion of the third conduit comprises a means for bringing the sulphur dioxide gas in the first conduit and the water in the second conduit into contained, codirectional flow into contact with each other. The majority of water used to create sulphurous acid in the system and method is introduced into the third conduit and flows through one or more mixing portions in the third conduit, thereafter discharging naturally by gravity and water flow.

10      Water is introduced into the third conduit in codirectional flow with the sulphur dioxide gas so as to create an annular column of water with the sulphur dioxide gas flowing inside the annular column of water thereby blending the water and sulphur dioxide gas together. In the preferred embodiment, water is introduced into the gas pipeline and passes through an eductor or venturi, which causes sulphur dioxide gas to be drawn through the first conduit without the need of pressuring the sulphur dioxide gas and without using an exhaust fan. The water and sulphur dioxide gas remain in contact with each other for the period of time it takes to flow through a portion of the third conduit. In the contact area, a portion of the sulphur dioxide gas reacts with the water, creating sulphurous acid.

20      In different embodiments, an agitation portion comprises a means for mixing and agitating the codirectionally flowing sulphur dioxide gas and water/sulphurous acid. The agitation portions enhance sulphur dioxide gas reaction and dispersion. Bends in or a length of the third conduit or obstructions within the third conduit are contemplated as means for mixing and agitating in the agitation portion. Agitation of the codirectional flow of the sulphur dioxide gas and water further facilitates reaction of the sulphur dioxide gas with water. Sulphurous acid and sulphur dioxide gas flow out of the third conduit through means for discharging the sulphurous acid and unreacted sulphur dioxide gas.

A discharge outlet represents a possible embodiment of means for discharging the sulphurous acid and unreacted sulphur dioxide gas. The discharge outlet permits conduit contents to enter into the subject aqueous solution to be treated, a holding tank therefor, or into further optional treatment apparatus such as a gas submersion zone.

5      Further Optional Features

The sulphurous acid and unreacted sulphur dioxide gas may exit the third conduit through the discharge and enter a gas submersion zone or mixing tank. In one embodiment, a weir divides the mixing tank into two sections, namely a pooling section and an effluent or outlet section. Sulphurous acid and sulphur dioxide gas exit the discharge of the third conduit into the pooling section. As the sulphurous acid pours into the mixing tank, it creates a pool of sulphurous acid equal in depth to the height of the weir. At all times, the water/acid and unreacted sulphur dioxide gas discharge from the third conduit above the level of the liquid in the pooling section of the mixing tank. In another embodiment, water/acid and unreacted sulphur dioxide gas discharge from the third conduit to mix in a single cell mixing tank, discharging out the bottom of the mixing tank.

In other words, the discharge from the third conduit is positioned sufficiently high in the mixing tank so that sulphur dioxide gas exiting the pipeline can pass directly into and be submerged within the pool while in an open (nonclosed) arrangement. In other words, the discharge from the third conduit does not create any significant back pressure on the flow of sulphurous acid or sulphur dioxide gas in the third conduit or gas pipeline. Nevertheless, the vertical position of the discharge from the third conduit into the pool reduces the likelihood that the unreacted sulphur dioxide gas will exit from the discharge without being submerged in the pool. In one embodiment, the discharge is removed a distance from the sidewall of the mixing tank toward the center of the pooling section to allow the pool to be efficiently churned by the inflow of sulphurous acid and unreacted sulphur dioxide gas from the third conduit. In another

embodiment, discharge out the bottom of the mixing tank upstream from a u-trap efficiently churns unreacted sulphur dioxide gas with the aqueous fluid of the system.

As acidic/water and gas continue to enter the mixing tank from the third conduit in one embodiment, the level of the pool eventually exceeds the height of the weir. Sulphurous acid spills over the weir and into the effluent or outlet section of the mixing tank where the sulphurous acid exits the mixing tank through an effluent outlet. The top of the effluent outlet is positioned below height of the weir and below the discharge from the third conduit in order to reduce the amount of free floating unreacted sulphur dioxide gas exiting the chamber through the effluent outlet. In another embodiment, a discharge in the bottom of a weirless mixing tank employs the column of water to inhibit unreacted sulphur dioxide from exiting the mixing chamber through the bottom discharge outlet. Free floating, unreacted sulphur dioxide gas remaining in the mixing tank rises up to the top of the mixing tank. The top of the mixing tank is adapted with a lid. Undissolved sulphur dioxide gas flowing through the effluent outlet are trapped by a standard u-trap, forcing accumulated gas back into the mixing tank while sulfurous acid exits the system through a first discharge pipe.

To ensure further elimination of any significant emissions of sulphur dioxide gas from the generator into the environment, the sulphur dioxide gas remaining in the mixing tank may be drawn into an exhaust conduit coupled with an exhaust vent on the lid of the mixing tank. The exhaust conduit defines a fourth conduit. Positioned in the fourth conduit is a means for introducing water into the fourth conduit. The water which enters the fourth conduit may be brought from a water source by any means capable of delivering sufficient water to the fourth conduit. As the water is introduced into the fourth conduit, it reacts with the sulphur dioxide gas that has migrated out through the lid of the mixing tank of the absorption tower, and creates sulphurous acid.

In the preferred embodiment, water introduced into the fourth conduit, passes through a second eductor or venturi causing the sulphur dioxide gas to be drawn through the vent and

into the fourth conduit. The gas and water are contained in contact as they flow in codirectional flow through one or more contact secondary containment and/or agitation portions of the fourth conduit. Sulphurous acid exits the fourth conduit through a second discharge pipe. The fourth conduit may be constructed of high density polyethylene plastic, pvc or any suitably durable plastic. The material of construction is chosen for its durability and resistance to ultra violet ray degradation. In a preferred embodiment, the second discharge pipe also comprises a u-trap configuration. In any discharge arrangement, the discharge of sulphurous acid may be into a holding tank from which the sulphurous acid may be drawn, injected or released into the subject aqueous solution.

In a preferred embodiment upstream from the u-trap of the second discharge pipe, a vent stack houses an exhaust scrubbing tower providing a tertiary containment area. The exhaust scrubbing tower defines grill holes through which the rising, undissolved gases rise. In a preferred embodiment, the exhaust scrubbing tower comprises a cylindrical body which is constructed of polyethylene plastic which is durable, lightweight and resistant to ultra violet ray degradation. At the top of the exhaust scrubbing tower, a third source of water introduces a shower of water through an emitter inside the exhaust tower showering water downward, resulting in a countercurrent flow of undissolved gases and descending water. The rising sulphur dioxide gas comes into countercurrent contact with the descending water, creating sulphurous acid.

The exhaust scrubbing tower is packed with path diverters, which force the countercurrent flow of sulphur dioxide gas and water to pass through a tortuous maze, increasing the duration of time the gas and water remain in contact and the surface area of the contact. Substantially all the free floating sulphur dioxide gas from the mixing tank will react with water in the tower to form sulphurous acid. Sulphurous acid created in the tower flows down into the secondary discharge. Any undissolved gases pass out of the open, upward end of the exhaust scrubbing tower to the atmosphere.

As mentioned, the water introduced into the system to the third conduit, fourth conduit and exhaust scrubbing tower may be brought from a water source to the system by any means capable of delivering sufficient water and pressure, such as a standing, elevated water tank, or mechanical, electric or diesel powered water pump.

5 The present invention also contemplates means for controlling the burn rate of sulphur in the burning chamber, that is, dampening the flow or amount of air made available into the burning chamber.

It is an object of this invention to provide sulphur gas or a sulfurous acid generator that is simple to manufacture, use, maintain and service.

10 Another object of this invention is to provide on-site, on-demand sulphur gas generation avoiding the expense, equipment, hazardous material management and personnel needed by the prior art methods and apparatus.

Another object of the present invention is to provide sulphur gases or sulfurous acid for aqueous water treatment or landfill treatment methods.

Still another object of the present invention is to provide an effective, efficient, easy to use method and apparatus to dechlorinate water.

It is also an object of this invention to construct the hopper and burn chamber out of a high-temperature concrete to reduce manufacturing costs.

20 It is another object of this invention to eliminate reliance upon countercurrent absorption as the prior mechanism for creating sulfurous acid as taught by the prior art.

It is further an object of this invention to create a sulfurous acid generator that is capable of operating without any electrical equipment such as pumps, air compressor or exhaust fans requiring a specific energy source requirement, such as electricity or diesel fuels.

25 It is another object of this invention to produce a sulfurous acid generator which converts substantially all sulfur dioxide gas generated into sulfurous acid.

It is another object of the invention to produce a sulfurous acid generator which uses an induced draw created by the flow of water through the system to draw gases through the otherwise open system.

Another object of the present invention is to provide a sulphurous acid generator with  
5 one or more contact containment and/or agitation and mixing mechanisms to increase the  
duration of time during which the sulphur dioxide gas is in contact with and mixed with water.

It is an object of this invention to produce a sulphurous acid generator which substantially eliminates emission of harmful sulphur dioxide gas.

These and other objects and features of the present invention will become more fully apparent from the following description and appended claims, or may be learned by the practice of the invention as set forth hereinafter.

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## BRIEF DESCRIPTION OF THE DRAWINGS

In order that the manner in which the above-recited and other advantages and objects of the invention are obtained, a more particular description of the invention briefly depicted above will be rendered by reference to a specific embodiment thereof which is illustrated in the appended drawings. With the understanding that these drawings depict only a typical embodiment of the invention and are not therefore to be considered to be limiting of its scope, the invention will be described and explained with additional specificity and detail through the use of the accompanying drawings in which:

Figure 1 is a perspective view of one embodiment of the sulphurous acid generator.

Figure 1A is a plan view of a section of a hopper and burn chamber.

Figure 1B is a cross-section of a hopper and burn chamber.

Figure 2 is a side elevation view partly in cutaway cross-section of the components of the sulphurous acid generator.

Figure 3 is a side elevation view partly in cut-away cross-section of an alternative embodiment of a sulphurous acid generator.

Figure 4A is a view partly in cut-away cross-section of an embodiment of a sulphur gas generator and injector.

Figure 4B is a side elevation view partly in cut-away cross-section of an embodiment of a sulphurous acid generator.

Figure 4C is a cross-sectional view partly of the Sagggregate™ concrete embodiment of a sulphur gas generator and injector.

Figure 5 is an enlarged view of a portion of a third conduit.

Figure 6 is an enlarged view of a portion of a fourth conduit.

Figure 7 is a cross-sectional view of the exhaust scrubbing tower.

Figures 8A to 8E illustrate alternative embodiments dampening available air or oxygen flowing into the burning chamber for combustion.

Figure 9 is a flow chart explaining one of the inventive processes.

Figure 10 is a flow chart explaining one of the inventive processes.

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**DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS**

Including by reference the figures listed above, applicant's sulphur gas and sulfurous acid generator comprises a system which generates sulphur dioxide gas and in some embodiments keeps the gas substantially contained and in contact with water or other aqueous solution for sufficient periods of time to substantially eliminate any significant release of harmful sulphur dioxide gas from the system or solution. The principal elements of the present invention are shown in Figures 1-8.

The sulphur or sulfur hopper 20 comprises enclosure 24 with a lid 26. Hopper 20 serves as a reservoir for elemental sulphur. Lid 26 may define a closeable aperture, not shown. Enclosure 24 may be of any geometric shape; square is shown, cylindrical may also be employed. Lid 26 of enclosure 24 is readily removable to allow sulphur to be loaded into hopper 20. Enclosure 24 defines a hopper outlet 30. Hopper 20 is configured such that sulphur in hopper 20 is directed toward hopper outlet 30 by the pull of gravity. Hopper outlet 30 allows sulphur to pass through and out of hopper 20.

Figure 1A illustrates a plan view of open hopper 20. Hopper 20 comprises a base or floor 22. In the preferred embodiment, a cooling ring 28 is disposed about  $\frac{1}{2}$  inch above base 22. As shown in Figure 1, untreated irrigation water is circulated through cooling ring 28. See also Figure 1B. Figures 1A and 1B also disclose vertical standing baffles 29. In practice of the invention it has been discovered that baffles 29 assist in directing the dry sulphur to hopper outlet 30. Practice of the invention has also revealed that cooling ring 28 is most effective when placed closer to hopper outlet 30 rather than the middle of base 22 or farther away from hopper outlet 30. The effect cooling ring 28 has on molten sulphur will be discussed below.

A passageway conduit 36 communicates between hopper outlet 30 and burn chamber inlet 50 of burn chamber 40.

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Burn chamber 40 comprises floor member 42, chamber sidewall 44 and roof member 46. Elemental sulphur is combusted in burn chamber 40. Roof member 46 is removably attached to chamber sidewall 44 supporting roof member 46. Roof member 46 defines an ignition inlet 52 as having a removably attached ignition inlet cover 54. Through ignition inlet 52, the user may ignite the sulphur. An air inlet 56 defined by chamber sidewall 44 has a removably attached air inlet cover 58. The air inlet 56 preferably enters the chamber sidewall 44 tangentially. An exhaust opening 60 in the burn chamber 40 is defined by the roof member 46.

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As shown in Figures 2, 3, and 4A-4C, roof member 46 also defines a downwardly extending annular ring 48. In the preferred embodiment, ring 48 extends downwardly into burn chamber 40 at least as low as air inlet 56 is disposed. It is understood and believed that this configuration causes not only inlet air to swirl in a cyclone effect into burn chamber 40 but induces a swirling or cyclone effect of the combusted sulphur dioxide gas as it rises in burn chamber 40 and passing up through exhaust opening 60 and gas pipeline 70. Roof member 46 is secured to sidewall 44 of burn chamber 40 by either bolting roof member 46 to burn chamber to the top of sidewall 44 in any conventional fashion, or as shown in Figure 4C, by employing removable C-clamps 49.

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Hopper 20, passageway conduit 36 and burn chamber 40 may be constructed of stainless steel. In such case, roof member 46 could be removably bolted to burn chamber 40. In an alternative embodiment shown in Figure 4C, hopper 20, passageway conduit 36 and burn chamber 40 as well as a platform or legs 10 may be constructed of Sagggregate™ concrete. Sagggregate™ concrete is a unique blend of cement and other components. The Sagggregate™ concrete comprises a cement component, two aggregate components, and a water component. The preferred cement component is Lumnite MG® (“Lumnite® cement”), Heidelberger Calcium Aluminate Cement from Heidelberger Calcium Aluminates, Inc., Allentown, Pennsylvania, United States of America. The preferred Lumnite® has a 7000 pound crush weight nature. The first aggregate is preferably a pea-sized medium shale sold by Utelite Corp.,

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Wanship, Utah, 84017, United States of America. A second aggregate is preferably a crushed mesh or crushed fines inorganic aggregate. The preferred fine-sized aggregate is PAKMIX® Lightweight Soil Conditioner® produced by Utelite Corp., Wanship, Utah, 84017, United States of America. The Pakmix® aggregate comprises No. 10 crushed fines of shale capable of bearing temperatures up to 2000 degrees Farenheit.

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The mixing ratio of the cement, first aggregate, second aggregate and water are as follows. The ratio of Lumnite® cement to combined aggregates is 1:3 by volume. The ratio of water to Lumnite® cement by weight is .4:1. Operational results are achieved when the volume ratio of pea-sized medium shale aggregate to Lumnite® cement ranges from about 0:1 to about 3.0:1 and where the volume ratio of crushed mesh/crushed shale fines aggregate to Lumnite® cement ranges from about 0:1 to about 3.0:1. More satisfactory results are achieved when the volume ratio of pea-sized medium shale aggregate to Lumnite® cement ranges from about 1:1 to about 1.5:1 and where the volume ratio of crushed mesh/crushed shale fines aggregate to Lumnite® cement ranges from about 1.5:1 to about 2.0:1. The most favorable results occur when the pea-sized medium shale aggregate is mixed in a ratio to Lumnite® cement in a range from about 1.2:1 to about 1.3:1 by volume and wherein the crushed mesh/crushed shale fines aggregate component is present in a ratio to Lumnite® cement in a range from about 1.7:1 to about 1.8:1 by volume.

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Embodiments of the Saggregate™ concrete of the present invention discussed above and illustrated in Figure 4 were made in the following manner:

EXAMPLE 1

<u>Component</u>	<u>Amount</u>
Lumnite® cement	one volume unit
pea-sized medium shale	1.5 x one volume unit
crushed fine shale	1.5 x one volume unit
water	.4 x weight of one volume unit of Lumnite®

For example, one cubic foot of Lumnite® cement is measured and weighed, the weight of one cubic foot of Lumnite® cement being noted. Measure one and one-half cubic feet of pea-sized medium shale. Measure one and one-half cubic feet of crushed fine shale. Mix the Lumnite® cement, pea-sized medium shale and crushed fine shale together to create a dry mix. Measure an amount of water equal to .4 times the weight of the one cubic foot of Lumnite® cement. Add the amount of water to the dry mix to create Sagggregate™ concrete. Mix, handle, pour, cure and treat the Sagggregate™ concrete like conventional concrete. In the context of the present invention, Sagggregate™ concrete was used with suitable molds to form the desired hopper-burn chamber assembly capable of withstanding the heat of burning and molten sulphur in use.

Other embodiments of the Sagggregate™ concrete of the present invention discussed above and illustrated in Figure 4 may be made in the following manner:

EXAMPLE 2

<u>Component</u>	<u>Amount</u>
Lumnite® cement	one volume unit
pea-sized medium shale	3.0 x one volume unit
crushed fine shale	None
water	.4 x weight of one volume unit of Lumnite® cement

For example, one cubic foot of Lumnite® cement is measured and weighed, the weight of one cubic foot of Lumnite® cement being noted. Measure three cubic feet of pea-sized medium shale. Use no crushed fine shale. Mix the Lumnite® cement and pea-sized medium shale together to create a dry mix. Measure an amount of water equal to .4 times the weight of the three cubic feet of Lumnite® cement. Add the amount of water to the dry mix to create Saggregate™ concrete. Mix, handle, pour, cure and treat the Saggregate™ concrete like conventional concrete. In the context of the present invention, Saggregate™ concrete is used with suitable molds to form the desired hopper-burn chamber assembly capable of withstanding the heat of burning and molten sulphur in use.

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### EXAMPLE 3

<u>Component</u>	<u>Amount</u>
Lumnite® cement	one volume unit
pea-sized medium shale	None
crushed fine shale	3.0 x one volume unit
water	.4 x weight of one volume unit of Lumnite® cement

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For example, one cubic foot of Lumnite® cement is measured and weighed, the weight of one cubic foot of Lumnite® cement being noted. Use no pea-sized medium shale. Measure three cubic feet of crushed fine shale. Mix the Lumnite® cement and crushed fine shale together to create a dry mix. Measure an amount of water equal to .4 times the weight of the one cubic foot of Lumnite® cement. Add the amount of water to the dry mix to create Saggregate™ concrete. Mix, handle, pour, cure and treat the Saggregate™ concrete like conventional concrete. In the context of the present invention, Saggregate™ concrete is used with suitable molds to form the desired hopper-burn chamber assembly capable of withstanding the heat of burning and molten sulphur in use.

EXAMPLE 4

<u>Component</u>	<u>Amount</u>
Lumnite® cement	one volume unit
pea-sized medium shale	.4 x one volume unit
crushed fine shale	2.6 x one volume unit
water	.4 x weight of one volume unit of Lumnite® cement

For example, one cubic foot of Lumnite® cement is measured and weighed, the weight of one cubic foot of Lumnite® cement being noted. Measure .4 cubic foot of pea-sized medium shale. Measure 2.6 cubic feet of crushed fine shale. Mix the Lumnite® cement, pea-sized medium shale and crushed fine shale together to create a dry mix. Measure an amount of water equal to .4 times the weight of the one cubic foot of Lumnite® cement. Add the amount of water to the dry mix to create Sagggregate™ concrete. Mix, handle, pour, cure and treat the Sagggregate™ concrete like conventional concrete. In the context of the present invention, Sagggregate™ concrete is used with suitable molds to form the desired hopper-burn chamber assembly capable of withstanding the heat of burning and molten sulphur in use.

EXAMPLE 5

<u>Component</u>	<u>Amount</u>
Lumnite® cement	one volume unit
pea-sized medium shale	one volume unit
crushed fine shale	2.0 x one volume unit
water	.4 x weight of one volume unit of Lumnite®

For example, one cubic foot of Lumnite® cement is measured and weighed, the weight of one cubic foot of Lumnite® cement being noted. Measure one cubic foot of pea-sized medium shale. Measure two cubic feet of crushed fine shale. Mix the Lumnite® cement, pea-sized

medium shale and crushed fine shale together to create a dry mix. Measure an amount of water equal to .4 times the weight of the one cubic foot of Lumnite® cement. Add the amount of water to the dry mix to create Saggregate™ concrete. Mix, handle, pour, cure and treat the Saggregate™ concrete like conventional concrete. In the context of the present invention,  
5 Saggregate™ concrete is used with suitable molds to form the desired hopper-burn chamber assembly capable of withstanding the heat of burning and molten sulphur in use.

EXAMPLE 6

<u>Component</u>	<u>Amount</u>
Lumnite® cement	one volume unit
pea-sized medium shale	1.1 x one volume unit
crushed fine shale	1.9 x one volume unit
water	.4 x weight of one volume unit of Lumnite®

For example, one cubic foot of Lumnite® cement is measured and weighed, the weight of one cubic foot of Lumnite® cement being noted. Measure one and one-tenth cubic feet of pea-sized medium shale. Measure one and nine-tenths cubic feet of crushed fine shale. Mix the Lumnite® cement, pea-sized medium shale and crushed fine shale together to create a dry mix. Measure an amount of water equal to .4 times the weight of the one cubic foot of Lumnite® cement. Add the amount of water to the dry mix to create Saggregate™ concrete. Mix, handle, pour, cure and treat the Saggregate™ concrete like conventional concrete. In the context of the present invention, Saggregate™ concrete is used with suitable molds to form the desired hopper-burn chamber assembly capable of withstanding the heat of burning and molten sulphur in use.

EXAMPLE 7

<u>Component</u>	<u>Amount</u>
Lumnite® cement	one volume unit
pea-sized medium shale	1.2 x one volume unit
crushed fine shale	1.8 x one volume unit
water	.4 x weight of one volume unit of Lumnite®

For example, one cubic foot of Lumnite® cement is measured and weighed, the weight of one cubic foot of Lumnite® cement being noted. Measure one and two-tenths cubic feet of pea-sized medium shale. Measure one and eight-tenths cubic feet of crushed fine shale. Mix the Lumnite® cement, pea-sized medium shale and crushed fine shale together to create a dry mix. Measure an amount of water equal to .4 times the weight of the one cubic foot of Lumnite® cement. Add the amount of water to the dry mix to create Saggregate™ concrete. Mix, handle, pour, cure and treat the Saggregate™ concrete like conventional concrete. In the context of the present invention, Saggregate™ concrete is used with suitable molds to form the desired hopper-burn chamber assembly capable of withstanding the heat of burning and molten sulphur in use.

EXAMPLE 8

<u>Component</u>	<u>Amount</u>
Lumnite® cement	one volume unit
pea-sized medium shale	1.3 x one volume unit
crushed fine shale	1.7 x one volume unit
water	.4 x weight of one volume unit of Lumnite®

For example, one cubic foot of Lumnite® cement is measured and weighed, the weight of one cubic foot of Lumnite® cement being noted. Measure one and three-tenths cubic feet of pea-sized medium shale. Measure one and seven-tenths cubic feet of crushed fine shale. Mix the Lumnite® cement, pea-sized medium shale and crushed fine shale together to create a dry mix.

Measure an amount of water equal to .4 times the weight of the one cubic foot of Lumnite® cement. Add the amount of water to the dry mix to create Sagggregate™ concrete. Mix, handle, pour, cure and treat the Sagggregate™ concrete like conventional concrete. In the context of the present invention, Sagggregate™ concrete is used with suitable molds to form the desired hopper-burn chamber assembly capable of withstanding the heat of burning and molten sulphur in use.

EXAMPLE 9

<u>Component</u>	<u>Amount</u>
Lumnite® cement	one volume unit
pea-sized medium shale	1.4 x one volume unit
crushed fine shale	1.6 x one volume unit
water	.4 x weight of one volume unit of Lumnite®

For example, one cubic foot of Lumnite® cement is measured and weighed, the weight of one cubic foot of Lumnite® cement being noted. Measure one and four-tenths cubic feet of pea-sized medium shale. Measure one and six-tenths cubic feet of crushed fine shale. Mix the Lumnite® cement, pea-sized medium shale and crushed fine shale together to create a dry mix. Measure an amount of water equal to .4 times the weight of the one cubic foot of Lumnite® cement. Add the amount of water to the dry mix to create Sagggregate™ concrete. Mix, handle, pour, cure and treat the Sagggregate™ concrete like conventional concrete. In the context of the present invention, Sagggregate™ concrete is used with suitable molds to form the desired hopper-burn chamber assembly capable of withstanding the heat of burning and molten sulphur in use.

The dry mix of Lumnite® cement and aggregates can be pre-mixed and bagged together. This greatly simplifies construction for the user because all components of the Sagggregate™ concrete are provided except water which can be provided on site. When mixed and cured, the

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Saggregate™ concrete is easily capable of withstanding the 400 to 600 degree Fahrenheit temperature of the burning and molten sulphur in burning chamber 40.

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In the preferred embodiment using Saggregate™ concrete to construct base 22 and sidewall 24 of hopper 20 should be 2½ to 3 inches thick. Similarly, the walls of the conduit passageway 36 and base 42 and sidewall 44 of burn chamber 40 should also have Saggregate™ concrete in the thickness of about 2½ to 3 inches. In the configuration shown in Figure 4C, lid 26 may be constructed of virtually any material, including wood, plastic, or any other material. Due to the extreme heat generated in burn chamber 40, roof member 46 must be made of a material that will withstand such extreme temperatures. Preferably, roof member 46 is constructed of stainless steel.

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As shown in Figure 4C, feet 10 may also be constructed of Saggregate™ concrete. Feet 10 are used to permit air to radiate under the bottom of hopper 20 and burning chamber 40 to dissipate radiant heat. As shown in Figures 1A, 1B and 4C, an additional advantage of placing cooling ring 28 in the hopper near passage conduit 36 results in a physical barrier and temperature barrier of any molten sulphur flowing from burning chamber 40 through conduit passageway 36 into hopper 20. In other words, the physical location of cooling ring 28 and the temperature gradient caused thereby, impedes the flow of any molten sulphur out of conduit passageway 36 so as to confine molten sulphur between cooling ring 28 and fluid conduit passageway 36. In a preferred embodiment, the hopper is in a square shape that has a cross-section of about 18 inches by 18 inches and is about 30 inches high in its inside dimensions. If a cylindrical shaped hopper is employed, an inside diameter of about 18 inches is preferred. In such a case, the inside height dimension of conduit passageway 36 is about 5 inches in inside height and about 10 inches in inside width with the burning chamber 40 being about 12 inches in height and having an inside diameter of 10 inches. This embodiment burns about 5 pounds of sulphur or less per hour and is capable of treating about 15 to 100 gallons of water per minute.

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In another larger embodiment, the hopper, if square, could have inside dimensions of about 32 inches by 42 inches, with a height of about 48 inches with the inside height dimension of conduit passageway 36 being about 6 inches in inside height and about 11 inches in inside width with a burn chamber having a height of about 16 inches and an inside diameter of about 18 inches. In this embodiment, tests have revealed that about 20 pounds of sulphur or less per hour is burned and the amount of water being treated may range from about 20 gallons per minute to about 300 gallons per minute.

The Saggregate™ hopper-chamber configuration of Figure 4C may be incorporated into the apparatus of Figures 1, 1A, 1B, 2 and 3.

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The present invention also contemplates a means for controlling the burn rate of sulphur in burn chamber 40. Figures 8A through 8E represent different means for dampening air intake through air inlet 56. Figure 8A illustrates a curved and/or occluded end of air inlet 56. Tests have revealed that a substantially centered hole having a diameter of about 1 to about 2 inches permits effective control of the burn of sulphur in chamber 40.

Figure 8B illustrates a conventional gate valve which can be placed along air inlet 56 to selectively dampen the flow of air into burn chamber 40.

Similarly, Figure 8C illustrates a conventional ball valve effective in restricting flow. Use of such a ball valve permits selective dampening or control of air through air inlet 56 into burn chamber 40.

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Figure 8D illustrates another embodiment in which a bend in air inlet 56 is followed by a ring disposed within air inlet 56 defining an opening 61 substantially perpendicular to the direction of flow of air. Air inlet 56 also has a second bend.

The preferred means for dampening the flow of air into burn chamber 40 is illustrated in Figure 8E. Air inlet 56 has a curve or bend and is packed with stainless steel mesh or wool.

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In all the embodiments of Figures 8A through 8E, air inlet 56 comprises a pipe or conduit having a diameter of about 3 inches.

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Sulphur supplied to the burn chamber 40 through the conduit inlet 50 can be ignited through the ignition inlet 52. The air inlet 56 allows oxygen, necessary for the combustion process, to enter into the burn chamber 40 and thus permits regulation of the rate of combustion. The exhaust opening 60 allows the sulphur dioxide gas to pass up through the exhaust opening 60 and into the gas pipeline 70.

#### Sulphur Gas Injector

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The present invention contemplates the introduction of sulphur gases directly into the water source to be treated such as a pressurized water line of an existing water system. These embodiments permit the sulphur gases to be drawn or injected into the existing water systems without the necessity, if desired, of pressurizing the sulphur gases.

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As illustrated in Figures 4A and 4C, direct injection embodiments are disclosed. In Figures 4A and 4C, sulphur is combusted in burner chamber 40. The combustion of sulphur and its attendant gas generation may be controlled as discussed above related to Figures 8A through 8E. In this way the sulphur gases can be generated on-site in an on-demand basis. Sulphur gases exit burn chamber 40 through exhaust opening 60. Sulphur gases pass through gas pipeline 70 to injector 310. Injector 310 is an injector which draws fluids or gases into a pressurized system at a point of differential pressure. The preferred injector 310 is a Mazzei™ Injector made by Mazzei Injector Corporation, Bakersfield, California, United States of America. Injector 310 operates upon water flow in an existing water line 300 having a flow of water. Injector 310 creates a differential pressure in line 300, across injector 310. The differential pressure draws or introduces sulphur gases in gas pipeline 70 into water line 300 without the necessity of pressurizing the sulphur gas. Injector 310 introduces the sulphur gas(es) directly into the water subject to treatment. This application is particularly suited to landfill application where it is desirable to spray or sprinkle acidic aqueous solution over landfill to treat and/or neutralize otherwise undesirable soils, waste, fertilizers and/or smells in cases where precision in solution of sulphur gases into aqueous solutions may vary. The devices and

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function of Figures 4A and 4C described herein provide means for passively introducing or injecting sulphur gases into a pressurized fluid line.

All of the foregoing burner chamber configurations permit the user to generate needed sulphur gases on-site thereby avoiding the costly purchase, transportation, and containment of preexisting sulphur gas delivery systems.

Sulphurous Acid Introducer

As already discussed, there are uses of sulphur gases known to those of skill in the art which uses do not require precise levels or amounts of dissolved or reacted sulphur gas(es) in aqueous solution or sulphurous acid in order to accomplish the desired chemical reaction or treatment or in order to avoid residual or offensive sulphur smells. Employing the burn chambers and air inlet dampeners discussed above, the present invention also contemplates a sulphur gas generator and introducer which simplifies the equipment or apparatus needed to controllably generate sulphurous acid on-site and on-demand. As disclosed in Figure 4B, the present invention contemplates introducing sulphurous acid into the subject water source without employing the mixing tank, and secondary and tertiary water introduction discussed below.

The gas pipeline 70 has two ends, the first end communicating with the exhaust opening 60, the second end terminating at a third conduit 76. The gas pipeline or first conduit 70 may comprise an ascending pipe 72 and a transverse pipe 74. The ascending pipe 72 may communicate with the transverse pipe 74 by means a first 90 degree elbow joint. Disposed about and secured to the ascending pipe 72 is a protective grate 90 to prevent unintended external contact with member 72 which is hot when in use.

Water is conducted through a second conduit 282 to a point at which the second conduit 282 couples with the first conduit 70 at a third conduit 76.

Conduit 76 comprises a means 100 for bringing the sulphur dioxide gas in the first conduit 70 and the water in second conduit 282 into contained codirectional flow. Water and

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sulphur dioxide gas are brought into contact with each other whereby sulphur dioxide gas dissolves into the water.

The codirectional flow means 100 shown in Figures 1, 2, 3, 4B and 5 comprises a central body 102, central body 102 defining a gas entry 104 and a sulfur dioxide gas exiting outlet 114, 5 central body 102 further comprising a secondary conduit inlet 106, and a water eductor 112. Eductor 112 generates a swirling annular column of water to encircle gas exiting outlet 114. The water flow, thermal cooling and reaction are believed to assist in drawing sulphur dioxide gas from burn chamber 40 into gas pipeline 70 where the gas is brought into contact with water to create sulphurous acid.

10 The codirection flow means 100 allows water to be introduced into the third conduit 76 initially through a second conduit inlet 106. The water entering the codirectional means 100 passes through the eductor 112 and, exits adjacent the sulphur dioxide gas outlet 114. The water enters the third conduit 76 and comes into contact with the sulphur dioxide gas by surrounding the sulphur dioxide gas where the sulphur dioxide gas and water are contained in contact with each other. The water and sulphur dioxide gas react to form an acid of sulphur. This first contact containment portion of conduit 76 does not obstruct the flow of the sulphur dioxide gas. It is believed that a substantial portion of the sulphur dioxide gas will react with the water in this first contact containment area.

20 If it is necessary or desirous to further agitate the codirectional flow of aqueous solution and gas to encourage and facilitate dissolution of sulphur gases into or reaction with the solution, an object 77 may be positioned inside third conduit 76 as shown in Figure 5 to alter the direction of the codirectional flow.

25 Third conduit 76 is disposed to discharge the flow of aqueous solution and undissolved sulphur gas(es), if any, through discharge 80 into the water source to be treated. In the preferred embodiment, discharge 80 is below the surface of the water source to be treated so as to permit further dissolution of undissolved sulphur gas(es) into the water source.

The sulphurous acid generator of Figure 4B, unlike the prior art, satisfactorily generates sulphur gases and sulphurous acid without excessive sulphur gas generation and smell because the amount of sulphur gases generated may be limited by employing the air inlet dampeners taught in relation to Figures 8A through 8E. By limiting or reducing the amount of sulphur gases generated, less sulphur gas is present, hence less sulphur is available and must be dissolved into or react with the solution. The preferred embodiment of gas pipeline 70 of Figures 4A, 4B and 4C is a two inch diameter pipe. In this way, less sulphur gas is generated and the available water is more able to host all or substantially all of the sulphur gas(es).

After the acid and any host water (hereafter “water/acid”) and any remaining unreacted gas continue to flow through third conduit 76, the water/acid and unreacted sulphur dioxide gas are mixed and agitated to further facilitate reaction of the sulphur dioxide with the water/acid. Means for mixing and agitating the flow of water/acid and sulphur dioxide gas is accomplished in a number of ways. For example, as shown in Figure 2, mixing and agitating can be accomplished by changing the direction of the flow such as a bend 84 in the third conduit 76. Another example includes placing an object 77 inside the third conduit 76 to alter the flow pattern in the third conduit 76 as shown in Figure 5. This could entail a flow altering wedge, flange, bump or other member 77 along the codirectional flow path in third conduit 76. By placing an object in the flow path, a straight or substantially straight conduit may be employed. The distinction of this invention over the prior art is mixing and agitating the flow of water/acid and sulphur dioxide in an open codirectionally flowing system. One embodiment of the present invention can treat between 20 and 300 gallons of water per minute coursing through third conduit 76 being held in contained contact with the sulphur dioxide gas.

After the water/acid and sulphur dioxide gas have passed through an agitation and mixing portion of third conduit 76, the water/acid and unreacted sulphur dioxide gas are again contained in contact with each other to further facilitate reaction between the components to create an acid of sulphur. This is accomplished by means for containing the water/acid and

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sulphur dioxide gas in contact with each other. One embodiment is shown in Figure 2 as a portion 85 of third conduit 76. Portion 85 acts much in the same way as the earlier described contact containment portion.

As shown in Figure 2, additional means for mixing and agitating the codirectional flow of water/acid and sulphur dioxide gas is employed. One embodiment is illustrated as portion 86 of third conduit 76 in which again the directional flow of the water/acid and sulphur dioxide gas is directionally altered. In this way, the water/acid and sulphur dioxide gas are forced to mix and agitate, further facilitating reaction of the sulphur dioxide gas to further produce or concentrate an acid of sulphur.

In the embodiment shown in Figure 2, third conduit 76 also incorporates means for discharging the water/acid and unreacted sulphur dioxide gas from third conduit 76. One embodiment is shown in Figure 2 as discharge opening 80 defined by third conduit 76. Discharge opening 80 is preferably positioned approximately in the center of the pooling section, described below. In the preferred embodiment, discharge 80 is configured so as to direct the discharge of water/acid and unreacted sulphur dioxide gas downward into a submersion pool 158 without creating a back pressure. In other words, discharge 80 is sufficiently close to the surface 133 of the fluid in the submersion pool to cause unreacted sulphur dioxide gas to be forced into the submersion pool, but not below the surface of the fluid in the submersion pool, thereby maintaining the open nature of the system and to avoid creating back pressure in the system.

As illustrated in Figure 2, one embodiment of the present invention also utilizes a tank 130 having a bottom 132, a tank sidewall 134, and a lid 164. Tank 130 may also comprise a fluid dispersion member 137 to disperse churning sulphurous acid and sulphur dioxide gas throughout tank 130. Dispersion member 137 may have a conical shape or any other shape which facilitates dispersion. A weir 148 may be attached on one side to the bottom member 132 and is attached on two sides to the tank sidewall 134. The weir 148 extends upwardly to a

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distance stopping below the discharge 80. The weir 148 divides the mixing tank 130 into a submersion pool 158 and an outlet section 152. The third conduit 76 penetrates either tank sidewall 134 or lid 164 (not shown). An outlet aperture 154 is positioned in the tank sidewall 134 near the bottom member 132 in the outlet section. The drainage aperture 154 is connected to a drainage pipe 156. Drainage pipe 156 is adapted with a u-trap 157. U-trap 157 acts as means to trap and force undissolved gases in a submersion zone, including sulphur dioxide gas, back into chamber 130 to exit through lid 164 into vent conduit 210. Sulphurous acid exits pipe 156 or primary discharge.

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As water/acid flows out of the third conduit 76, the weir 148 dams the water/acid coming into the mixing tank 130 creating a churning submersion pool 158 of sulphurous acid. Sulphur dioxide gas carried by but not yet reacted in the sulphurous acid is carried into submersion pool of acid 158 because of the proximity of the discharge 80 to the surface 133 of the pool 158. The carried gas is submerged in the churning submersion pool 158. The suspended gas is momentarily churned in contact with acid in pool 158 to further concentrate the acid. As unreacted gas rises up through the pool, the unreacted gas is held in contact with water and further reacts to further form sulphurous acid. The combination of the discharge 80 and its close proximity to the surface 133 of pool of acid 158 creates a means for facilitating and maintaining the submersion of unreacted sulphur dioxide gas discharged from the third conduit into the submersion pool of sulphurous acid to substantially reduce the separation of unreacted sulphur dioxide gas from contact with the sulphurous acid to promote further reaction of the sulphur dioxide gas in the sulphurous acid in an open system without subjecting the sulphur dioxide gas discharged from the third conduit to back pressure or system pressure. That is, discharge 80 positions below the level of the top of weir 148 is contemplated as inconsistent with the open system illustrated by Figure 2. However, discharge 80 may be positioned below 20 the level of the top of weir 148 or below the surface 133 of submersion pool 158.

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As sulphurous acid enters the mixing tank 130 from the third conduit 76 the level of the pool 132 of sulphurous acid rises until the acid spills over the weir 148 into the outlet section 152. Sulphurous acid and sulphur dioxide gas flow out of the mixing tank 130 into the drainage pipe 156. Drainage pipe 156 is provided with a submersion zone in the u-trap 157 in which sulphur dioxide gas is again mixed into the sulphurous acid and which prevents sulphur dioxide gas from exiting the drainage pipe or primary discharge 156 in any significant amount.

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Referring to the embodiment illustrated in Figure 3, first conduit 70 and second conduit 282 are coupled as discussed above. However, in this embodiment, third conduit 76 may have a bend 84 to transition to length 85 and define a discharge opening 80 into mixing tank 130. As shown in this embodiment, the water/acid and undissolved sulphur dioxide enter the mixing tank in a downward angle direction. Another embodiment, not shown, contemplates third conduit 76 entering directly into the top of mixing chamber 130 through lid 164.

Mixing tank 130 of the embodiment of Figure 3 comprises a bottom member 132 defining an outlet aperture 154. Mixing tank 130 has a diameter of about 6 to 8 inches. As a result, the inside volume of mixing tank 130 is such that as water/acid begins to fill tank 130 and interacts with u-trap 157, the level of water/acid rises and falls in a flushing action.

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As water/acid discharges from third conduit 76 into mixing tank 130, it results in a turbulent washing machine effect forcing undissolved sulphur dioxide gas into the churning water/acid in mixing tank 130. As depicted in Figure 3, u-trap 157 extends vertically a distance up into mixing tank 130 through floor member 132. This configuration provides a further agitation zone 131 in which descending waters/acid must change its direction and ascend in tank 130 before exiting out u-trap 157. As a result, submersion pool 158 in use represents a churning pool wherein undissolved sulphur dioxide is contained in water/acid for further dissolution and/or in u-trap 157 acts to trap and direct undissolved gases back up through submersion pool 158 to escape out exhaust vent 202 and enter into vent conduit 210. On the other hand, sulphurous acid exits the system through drainage pipe or primary discharge 156.

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For the embodiments shown in both Figures 2 and 3, any free floating sulphur dioxide gas in mixing tank 130 rises up to the lid 164. The lid 164 defines an exhaust vent 202. Exhaust vent 202 may be coupled with a vent conduit 210. The vent conduit 210 has a first end which couples with the exhaust vent 202 and a second end which terminates at a fourth conduit 220. The vent conduit 210 may consist of a length a pipe between vent 202 and the fourth conduit 220. The fourth conduit 220 comprises auxiliary means 240 for bringing sulphur dioxide gas in the vent conduit and substantially all the water in a supplemental water conduit 294 into contained, codirectional flow whereby remaining sulphur dioxide gas and water are brought into contact with each other. See also Figure 6.

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As shown in Figures 2, 3 and 6, the auxiliary means has a body 240 defining a gas entry 244, a gas outlet 252, a supplemental water conduit inlet 246, and water eductor 250.

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Water enters the auxillary means 240 through the supplemental water conduit 294 at inlet 246. The water courses through inlet 246 and eductor 250 as discussed earlier as to the codirectional means. Water eductor 250 draws any free floating sulphur dioxide gas into the exhaust vent conduit 210. Water and sulphur dioxide gas are brought into contact with each other in fourth conduit 220 by surrounding the gas exiting gas outlet 252 with water exiting eductor 250. The water and gas are contained in contact with each other as the gas and water flow down through fourth conduit 220 to react and form an acid of sulphur. This contact containment area does not obstruct the flow of the sulphur dioxide gas. It is believed that substantially all of the remaining sulphur dioxide gas in vent conduit 210 reacts with the water in this contact containment area.

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In fourth conduit 220, the water/acid and unreacted or undissolved sulphur dioxide gas also experience one or more agitation and mixing episodes. For example, as fluid and gas divert in fourth conduit 220 at elbow 262, the flow of water/acid and sulphur dioxide gas is mixed and agitated. The water/acid and sulphur dioxide gas are again contained in contact with each other thereafter. As a result, like the water/acid and sulphur dioxide gas in the third conduit 76, the

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water/acid and sulphur dioxide gas in fourth conduit 220 may be subject to one or more contact containment portions and one or more agitation and mixing portions. The fourth conduit may have a u-trap 267. U-trap 267 acts as means to cause bubbles of unabsorbed diatomic nitrogen gas or undissolved sulphur dioxide, if any, to be held or trapped on the upstream side of u-trap 267 in a submersion zone. Secondary discharge 264 may also be configured with a vent stack 265. Remaining diatomic nitrogen gas in the system is permitted to escape the system through vent stack 265. Operation of the system reveals that little, if any, sulphur dioxide escapes the system. It is believed that gas that is escaping the system is harmless diatomic nitrogen. This configuration of a sulphur acid generator eliminates the dependence upon use of a countercurrent absorption tower technology of the prior art to effect production of sulphurous acid. Nevertheless, as an added safety feature to, and to further diminish any possible sulphur smell emitting from a device, vent stack 265 may comprise a limited exhaust scrubbing tower.

As shown in Figures 2, 3, and 7, vent stack 65 encases two substantially horizontally placed vent screens 269. In the preferred environment, vent stack 265 is severable and connectable at joint 271. This facilitates construction shipment and maintenance. The upper vent screen 269 acts to contain path diverters 263 within vent stack 265. The source of water 295 is disposed to enter vent stack 265 at or near the top of vent stack 265. A water dispersion device 261 is attached to the end of water conduit 295 inside vent stack 265 above the column of path diverters 263. The preferred water dispersion device 261 is an i-Mini Wobbler distributed by Senninger Irrigation, Inc., Orlando, Florida, 32835, United States of America. In the present invention the water dispersion device 261 is, contrary to its intended use, inverted 180°. Experimentation has shown that the i-Mini Wobbler is the most effective in an inverted fashion because it duplicates rain in large droplets rather than a mist or spray and due to the wobbling affect of the device, it creates a randomly dispersed water flow thereby more effectively wetting the column of path diverters 263. This creates a water saturated

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tortuous path through which any undissolved gases trapped by u-trap 267 and venting out of discharge 264 must filter. In the preferred embodiment, the path diverters 263 are Flexirings® diverters 263. In this configuration, the only countercurrent flow of water and any undissolved gases is in the exhaust scrubbing tower of vent stack 265. Any water and sulphurous acid running out the bottom of vent stack 265 enter into discharge 256. In this way, these embodiments also provide means for controllably generating sulphurous acid on-site and on-demand.

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Experimentation has shown that the majority of water entering the system of the present invention enters at inlet 106. A lesser amount of water enters the system at inlet 246 with only a fraction of the water entering the system through conduit 295. The flow of sulphur dioxide gas and water through the apparatus/system is depicted in flow diagram Figure 9.

#### Sulphurous Acid Injector

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Unlike the prior art devices which release or pump sulphurous acid or water/acid back into water sources, the present invention also contemplates injecting the sulphurous acid discharged from discharges 156 and 264 into a desired, existing water source. The present invention requires, however, no pump or pressurized sulphurous acid generator to inject or discharge the discharged sulphurous acid into the desired body of water. The novel injection system relies instead upon an existing water line 300 which has sufficient flow so as to create the needed differential pressure across injector 310. The preferred injector is a Mazzei™ Injector. Injector 310 creates a differential pressure and is configured to draw liquid or gas into the flow within line 300 as discussed above.

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Injector 310 is located beneath a reservoir 320 which acts as a reservoir for sulphurous acid discharged from discharges 156 and 264. Injector 310 draws sulphurous acid from reservoir 320 and injects it into the fluid flow in line 300. Employing injector 310 as discussed above, the present invention provides a means for passively introducing or injecting sulphurous acid into a pressurized fluid line. The term “passively” means that the sulphur gases and/or

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sulphurous acid is not put under positive pressure to effect injection into line 300 but that in ambient conditions in gas pipeline 70 and in reservoir 320, the respective sulphur gas(es) or sulphurous acid is drawn into line 300 by injector 310.

Figures 1, 2 and 3 show a primary pump 280 supplying water through a primary  
5 hose 282 to the secondary conduit water inlet 106 at codirectional means 100. A supplemental or secondary pump 290 supplies water to auxiliary means 240 through a supplemental water conduit hose 294 and to conduit 295. It will be appreciated that any pump capable of delivering sufficient water to the system may be utilized and the pump may be powered by any source sufficient to run the pump. A single pump with the appropriate valving may be used or several pumps may be used. It is also contemplated that no pump is necessary at all if an elevated water  
10 tank is employed to provide sufficient water flow to the system or if present water systems provide sufficient water pressure and flow.

#### Dechlorinization of Aqueous Solution

The chemistry of dechlorinization of aqueous solution using sulphur gases is known. Unlike known technology, the present invention provides apparatuses, methods and means for controllably, inexpensively, safely and reliably generating the needed sulphur gases or acids of sulphur used to dechlorinate aqueous solution on-site and on-demand. By employing either the Sulphur Gas Injectors or the Sulphurous Acid Introducers disclosed above, the present invention provides heretofor unknown systems and methods capable of effecting dechlorinization of aqueous solution. The expensive and large tanks, tankers, rails, trains, trucks, containment,  
20 piping and other equipment needed by known systems and methods are entirely eliminated by the simple, self-contained, on-site, on-demand production of sulphur gases and/or sulphurous acids from the combustion of sulphur.

By utilizing the gas and acid generators and introducers of the present invention, water treatment plants or other facilities may inexpensively, safely and successfully dechlorinate water  
25 as needed to meet EPA and other safety and health requirements.

The present invention may be embodied in other specific forms without departing from its spirit or essential characteristics. The described embodiments are to be considered in all respects only as illustrative and not restrictive. The scope of the invention is, therefore, indicated by the appended claims rather than by the foregoing description. All changes which come within the meaning and range of equivalency of the claims are to be embraced within their scope.

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What is claimed and desired to be secured by United States Letters Patent is:

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